Molecular Catalysis Science

Nanoparticle synthesis and instrument development for characterization under reaction conditions: Conquering catalytic complexity by unifying the fields of catalysis

Colloidal chemistry is used to control the size, shape, morphology, and composition of metal nanoparticles. Model catalysts as such are applied to catalytic transformations in the three types of catalysts: heterogeneous, homogeneous, and enzymatic. Real-time dynamics of oxidation state, coordination, and bonding of nanoparticle catalysts are put under the microscope using surface techniques such as sum-frequency generation vibrational spectroscopy and ambient pressure X-ray photoelectron spectroscopy under catalytically relevant conditions. It was demonstrated that catalytic behavior and trends are strongly tied to oxidation state, the coordination number and crystallographic orientation of metal sites, and bonding and orientation of surface adsorbates. It was also found that catalytic performance can be tuned by carefully designing and fabricating catalysts from the bottom up. Homogeneous and heterogeneous catalysts, and likely enzymes, behave similarly at the molecular level. Unifying the fields of catalysis is the key to achieving the goal of 100% selectivity in catalysis.

Two major breakthroughs have revolutionized molecular catalysis science over the last 20 years. The first is in the development of nanomaterials science\(^1\)-\(^4\), which has made it possible to synthesize metallic\(^5\)-\(^7\), bimetallic, and core-shell nanoparticles\(^8,9\); mesoporous metal oxides\(^10,11\); and enzymatic particles\(^12\)-\(^16\) in the nanocatalytic range between 0.8 and 10 nm. The second innovation is in the advancement of spectroscopy and microscopy instruments\(^17\)-\(^20\) — including nonlinear laser optics\(^21\); sum-frequency generation vibrational spectroscopy\(^22\)-\(^24\); and synchrotron-based instruments, such as ambient pressure X-ray photoelectron spectroscopy\(^8,25\)-\(^27\), X-ray absorption near-edge structure, extended X-ray absorption fine structure\(^28\)-\(^30\),...
infrared (IR) and X-ray microspectroscopies\textsuperscript{31}, and high-pressure scanning tunneling microscopies\textsuperscript{32,33} — that characterize catalysts at the atomic and molecular levels under reaction conditions\textsuperscript{34}. Most of the studies that utilize these techniques focus on nanoscale technologies, such as catalytic energy conversion and information storage, which have reduced the size of transistors to below 25 nm\textsuperscript{35}.

Catalysts are classified into three types — heterogeneous, homogeneous, and enzymatic — and in most cases range in size from 1 to 8 nm, which is even smaller than the transistors being developed by the latest size-fabrication technologies. Heterogeneous catalysts work in reaction systems with multiple phases, e.g., solid-gas or solid-liquid phase; homogeneous catalysts reside in the same phase as the reactants, almost always in the liquid phase; and enzymatic catalysts, which are most active in a buffer solution, make use of active sites in proteins. The catalysis of chemical energy conversion provides ever-increasing selectivity in producing combustible hydrocarbons, gasoline, and diesel.

The tenets that direct our catalysis research involve nanoparticle synthesis; characterization under reaction conditions; and reaction studies using these nanoparticles to determine kinetics, selectivity, deactivation, and other catalytic kinetic parameters. These are studied in the same research group as they are the underpinning of molecular catalysis. The hypothesis that we are striving to prove is that the three fields of catalysis (heterogeneous, homogeneous and enzyme) behave similarly on the molecular level. These ongoing studies as well as their success and future outlook are the subjects of this paper.

**Metal nanoparticles for size-dependent covalent bond catalysis**

The major technique for the synthesis of nanoparticle catalysts is colloid chemistry (Fig. 1a). These nanoparticle-based catalysts are produced with precisely controlled sizes in the 1-10 nm range in two dimensions using the Langmuir-Blodgett technique\textsuperscript{36} or placed on porous three-dimensional supports. The nanoparticles,
mostly metals, are placed in a microporous and mesoporous support. The mesoporous support is made with mesoporous silica between 5-25 nm pores coated by a transition metal oxide. The silica is removed by leaching with sodium hydroxide to leave behind a mesoporous template that is loaded up with nanoparticles used for catalytic studies. The oxide itself, as it will be shown, is often a very important ingredient for catalytic reactions\(^{34}\).

In our work, we found that the size and shape of metal nanoparticles control both catalytic reaction rates and selectivities. We also learned that all of these multipath reactions show size dependence in their turnover rates and selectivity\(^{37}\). It is possible to achieve different shapes of platinum nanoparticles (Fig. 1b) and the size regime of platinum nanoparticles can be sharply focused in the 1.5 to 8.0 nm range (Fig. 1c). Such a well-defined particle size and distribution are essential to detecting the turnover rates of the hydrogenation of either benzene or toluene, as they are structure sensitive. We also observed fourfold change in turnover rates between nanoparticles of platinum in the 2–4 nm range and in the 4–6 nm range. The size and shape dependence of nanoparticles can readily be controlled by colloid science technology\(^{36,38,39}\) (Fig. 1c). The isomerization of methylcyclopentane is much more shape dependent on the platinum nanoparticles than size dependent\(^{40}\) (Fig. 1d). In the case of the Fischer-Tropsch CO hydrogenation reaction, the product distribution is size dependent\(^{41}\) and the turnover rate increases fivefold with increasing size (Fig. 1e).

Previous studies only examined catalysts before use (i.e., as-made or pre-natal catalysts) and after use (i.e., spent or post-mortem catalysts) and thus could not determine how a metal nanocatalyst’s structure and other properties, including composition and oxidation states, would change as a function of reaction time, temperature, and pressure.

**Characterization under reaction conditions**
Engineering chemical and physical properties at molecular levels is a challenging task that requires tools and strategies known as *in situ* probing to characterize catalysts in action. This *in situ* method measures macroscopic and microscopic properties simultaneously or separately under identical or similar conditions in an attempt to correlate function and structure\textsuperscript{31}. In addition to this *in situ* approach, surface techniques — with temporal, spatial, and chemical resolutions in their respective scales of subsecond, subnanometer, and vibrational and electronic levels — are prerequisites to gaining molecular insight into catalysts’ operations\textsuperscript{42-44}. These techniques are often based on detecting outbound electrons, photons, or ions of catalysts of interest upon excitation with high-energy electrons or photons in a broad electromagnetic spectrum ranging from radio waves to IR and visible light, and to UV and X-rays. Monochromated in energies and collimated or focused in space, these probes carry electronic, vibrational, and bonding information, giving away fundamental details of the otherwise hidden components of a catalyst — pieces of a puzzle, and snapshots of a bigger picture.

Fig. 2a shows sum-frequency generation nonlinear optical spectroscopy\textsuperscript{24}, which is very sensitive to the surface adsorbed species under catalytic reaction conditions\textsuperscript{22-24,45}. Several molecular species are found\textsuperscript{23} on the surface during ethylene hydrogenation, cyclohexene hydrogenation, and dehydrogenation (Fig. 2b). While some species, as well as their turnover rates, change dynamically under these conditions, others are merely spectators. It is also clear that some of the reaction intermediates are neither the reactants nor the products but something in between. The mechanistic details are revealed by sum-frequency generation under reaction conditions.

Ambient pressure X-ray photoelectron spectroscopy (XPS) is shown\textsuperscript{8,25-27} schematically in Fig. 2c. Bimetallic nanoparticles are shown being studied by this technique. Palladium-rhodium bimetallic nanoparticles 15 nm in size show rhodium segregation under nitric oxide (NO)-adsorption-induced oxidizing conditions. Palladium catches up with rhodium surface composition when we add a
reducing gas — carbon monoxide (CO) — adsorbed on the surface. The outcome of these studies is to show that bimetallic nanoparticles undergo a surface composition change that is driven by dynamic chemical oxidizing and reducing environments (Fig. 2d).

A high-pressure scanning tunneling microscope (STM) shows that the adsorbates reacting on the catalyst surface are mobile under reaction conditions. For example, when cyclohexene hydrogenation and dehydrogenation turnovers are measured under reaction conditions, the STM image is diffused. This indicates that the adsorbate molecules move at a faster rate than the scanning tunneling tip’s surface motion of 100 Å per millisecond. However, if the surface is contaminated by carbon monoxide adsorption, cyclohexene hydrogenation and dehydrogenation reaction turnovers come to a halt, and an ordered surface structure forms, which is readily detectable by STM. We observed that not only are the adsorbed molecules mobile under catalytic reaction conditions, but the adsorbate-induced restructuring of the metal surfaces are also enhanced by high reactant pressures. The stepped platinum single crystal surfaces becoming clustered and rearranged at high-pressure carbon monoxide adsorption (Fig. 3a). This clustered formation is reversible, however: when carbon monoxide is removed from the surface by evacuation, the stepped structure of the original crystal surface is reestablished.

**Oxidation state of nanoparticles change with decreasing size: Conversion of heterogeneous to homogeneous catalysis**

When CO oxidation was studied on rhodium nanoparticle surfaces as a function of size below 2 nm, the CO oxidation rates increased by thirtyfold. Ambient pressure XPS studies indicated that the higher turnover rates are due to the oxidation state of rhodium changing from metallic rhodium to rhodium (Fig. 3b). Similar studies on platinum indicated that platinum nanoparticles above 1.5 nm are metallic; however, the studies also found that platinum below 1.5 nm and as low as 0.8 nm are in the 2⁺ and 4⁺ oxidation states. Because very few bulk atoms are available
for these nanoparticles, they become dominated by low coordination surface atoms, and as a result, their electronic structure changes. Nørskov et al.\textsuperscript{48} have studied this process and found that the adsorption energy of oxygen on gold nanoparticles changes as a function of a decrease in size. Because there is a decrease in the gold coordination number at the adsorption sites and fewer than 55 atoms, which is slightly more than 1 nm, the gold becomes oxidized to gold 1\textsuperscript{+} and 3\textsuperscript{+} instead of metallic gold.

The homogeneous catalysts are usually single transition metal ions, surrounded by ligands. As a result, we tried to use these small nanoclusters, which have controlled high oxidation states to carry out homogeneous catalysis. We adsorbed the small nanoclusters on dendrimers, treelike polymers that hold these nanoparticles throughout its branches. We found that these are excellent homogeneous catalysts, so we managed to heterogenize homogeneous reactions by using nanoparticles composed of 40 atoms of rhodium, palladium, gold, or platinum for reactions including hydroformylation, decarbonylation, and other commonly known homogeneous catalytic reactions\textsuperscript{3,31,47}. X-ray absorption spectroscopy studies (XANES and EXAFS) showed\textsuperscript{28-30} that the nanoparticles dispersed to small low coordination clusters under oxidizing conditions, but reassembled to the original 1 nm particles when under reduction by reactants, products, or the dendrimers. This process is also reversible.

Likewise, single site homogeneous catalysts are low coordination systems comprised of ligands that control electronic structure and chemistry at the molecular level\textsuperscript{29,49} (Fig. 3c). By controlling types and binding of ligands, a high level of selectivity (regio- and enantio-selectivity) is obtained in homogenized catalytic reactions. Capping agents used in colloidal synthesis, similar to ligands in single site organometallic complexes, can be utilized to control selectivity in heterogenized homogeneous reactions, which, as of today, remains a great challenge.

**Oxide-metal interfaces as active sites for acid-base catalysis**
Platinum is an excellent hydrogenation catalyst of many organic molecules, such as crotonaldehyde. When platinum nanoparticles of the same size are placed on two different oxides — silica and titania — one can see that the turnover rates and the selectivities are much higher when titania rather than silica is used as a support. The importance of the oxide support for metal catalysts to change selectivities and product distributions is well known. This phenomenon of the oxide support effect on catalytic reaction rates where the oxide alone does not carry out the same or any reaction is called positive strong metal support interaction (SMSI) in the literature\(^\text{50}\). It is the charge transfer ability of reducible oxide supports that acts on the performance of metal catalysts, but how does charge regulate catalytic processes?

An explanation was found by surface physics studies of hot electron emission under light illumination that was carried out by exothermic catalytic reactions on metal surfaces\(^\text{51}\), such as CO oxidation or hydrogen oxidation (Fig. 4a). The deposited energy produces high kinetic energy electrons that have a mean free path within the metal in the range of 5 to 10 nm. The chemical energy deposition in metals to produce hot electrons has been well demonstrated by Rettner, Auerbach, and Wodtke\(^\text{52}\) using highly vibrationally excited NO molecules impinging on gold as compared to lithium fluoride surfaces. On gold, the NO molecules in the 15\(^{\text{th}}\) vibrationally excited state lose 1.5 eV energy to produce molecules in the 8\(^{\text{th}}\) vibrational state. On the other hand, the vibrationally excited NO molecules lost no energy when they scattered from lithium fluoride, which has no free electrons. The hot electron generation can be observed by using exothermic catalytic reactions on a Schottky diode on platinum and titanium oxide where the platinum is less than about 5 nm in thickness. The charge flow between the platinum and the titanium oxide allows one to determine the current flow in the battery configuration shown in Fig. 4a. One can detect a so-called chemicurrent, which is correlated with the turnover rate of exothermic CO oxidation or hydrogen oxidation reactions\(^\text{53}\). Theoretical calculations showed that the transition state in these processes involves
CO₂ or H₂O, which yields to the chemicurrent that is proportional to the turnover rate.

Acid-base catalysis is correlated with charge concentration, and not with surface area, while covalent bond catalysis is surface area dependent. These two modes of catalysis are the major ways chemistry occurs in most catalytic processes. When one places metal nanoparticles into a mesoporous oxide support, many oxide-metal interfaces are produced within the mesopores between the metal and the oxide. Studies have found that these oxide-metal interfaces have major effects on catalytic reactions. The isomerization of n-hexane on naked oxide only results in the cracking of the n-hexane molecules, while mesoporous oxides give rise to 100% selectivity of n-hexane isomers of high octane numbers in the presence of platinum (Fig. 4b). The next figures (Fig. 4c-4e) shows similar effects when platinum is placed on various oxide mesopores. Platinum nanoparticles produce very little CO oxidation within mesoporous silica, but when they are placed on mesoporous cobalt oxide, more than a thousand fold increase in catalytic turnover for CO oxidation kinetics is found.

Fig. 4c (right) shows mesoporous transition metal oxide supported platinum nanoparticles. This is the oxide-metal interface, which produces large, strong metal support effects. There is a charge transfer between the metal and the oxide under reaction conditions. If the oxide is alone, as in the case of n-hexane conversion with pure oxides of niobium oxide, titanium oxide, and other oxides, only the cracking of the n-hexane molecules is observed. However, if the platinum is in the mesopores, a 100% selectivity to isomerization is produced, which is very high and an important factor in making high-octane gasoline.

Fig. 4c (left) shows platinum nanoparticles in contact with microporous oxides when the platinum nanoparticle is much larger and cannot fit into the micropores. In this case, the chemistry that occurs — known as bifunctional catalysis — is the sum total of the chemistry of platinum and the microporous oxide, which act in
parallel or consecutively. In the other case, when the mesoporous transition metal oxide can accommodate the 3 nm platinum inside its mesopores, there are oxide-metal interfaces — or single site catalysis — where the oxide-metal interface produces charges and acid-base catalysis, which is uniquely selective in many circumstances. Similar results are seen when CO oxidation is carried out on platinum supported by silica or another transition metal oxide\textsuperscript{55}. The turnover rate on silica is small, equal to pure platinum turnover; however, when cobalt oxide is the mesoporous support, the turnover rate is amplified by a thousand fold (Fig. 4e). This is indeed a major increase in catalytic activity.

**Hybrid systems: outlook**

It is clear that we can heterogenize homogeneous catalysts. However, enzymes\textsuperscript{12-16} are also very important catalytic systems, and recent studies have focused on how to synthesize pure enzymes as well as on how to look for similarities between enzymes and all three catalytic systems on the molecular scale. For example, it is known that enzymes can become more similar to heterogeneous catalysts when they are immobilized on a surface. We plan to advance previous work by studying enzymes at the molecular level and developing a molecular understanding of all three types of catalysts under similar conditions of reactions and chemical environment.

In our attempt to focus on the chemical correlations between the three catalysis groups — heterogeneous, homogeneous, and enzymatic — the future looks very promising for molecular catalysis science studies. Catalysis of homogeneous, heterogeneous, or enzymatic origin alike involvednanosized materials. These nanocatalysts are comprised of inorganic and/or organic components. Charge, coordination, interatomic distance, bonding, and orientation of catalytically active atoms are molecular factors shared by all three field of catalysis. By controlling the governing catalytic components and molecular factors, catalytic processes of a multichannel and multiproduct nature could be run in all three catalytic platforms.
to create unique end-products. This is the promise of a molecularly unified catalytic scheme of the future.

References


**Acknowledgements**

The work shown in this perspective article was supported by the Director, Office of Science, Office of Basic Energy Sciences, Chemical Sciences, Geosciences and
Biosciences Division of the US Department of Energy under Contract No. De-AC02-05CH11231.

Competing financial interests
The authors declare no competing financial interests.
Figure 1 | Examples of size and shape control of nanoparticles, and the effects on nanoparticle catalysts. a, Schematics of Pt nanoparticles synthesis by the polyl reduction method. b, TEM images and ball models of Pt nanoparticles with different shapes. c, Left: Particle size distribution histograms of the Pt/SBA-15 series catalysts.
obtained from TEM images. The number inserts indicate the mean particle diameter and standard deviation for each sample. Right: TEM and HRTEM images of Pt nanocrystals with different shape and size. TEM images of (A) 9 nm nanocubes, (C) 7 nm nanocubes, (E) 6 nm nanocubes, (G) 5 nm nanocubes, (I) 5 nm nanopolyhedra, and (K) 3.5 nm nuclei. HRTEM images of a single (B) 9 nm nanocube, (D) 7 nm nanocube, (F) 6 nm nanocube, and (H) 5 nm nanocube along the [100] zone axis. HRTEM images of a single (J) 5 nm nanopolyhedron, and (L) 3.5 nm nucleus along the [111] zone axis. The scale bars are 20 nm in the TEM images and 1 nm in the HRTEM images. 

d, Reaction pathways and possible products of methylcyclopentane hydrogenation reaction catalyzed by Pt nanoparticles with different shapes. 

e, Left: CO consumption turnover frequency for the CO hydrogenation at 5 bar (H₂:CO = 2:1) for various sizes of cobalt nanoparticles catalyst supported on MCF-17. The turnover frequency (TOF) corresponds to the number of CO molecules converted in time divided by the amount of cobalt atoms at the catalyst surface. Right: Selectivities toward hydrocarbons with a carbon number of 5 and higher (C5+) and methane selectivities (SCH₄) as a function of cobalt crystallite sizes for hydrogenation of carbon monoxide (H₂:CO = 2:1) at 5 bar and 250 °C. Both selectivities are expressed relative to the total number of carbon atoms converted.

Figures adapted with permission from: b, ref. 36, ACS; c(left), ref. 38, Elsevier; c(right), ref. 39, ACS; d, ref. 40, Springer; e, ref. 41, Springer.
Figure 2 | *In situ* characterization of catalyst surfaces using SFG and XPS.

**a**, Schematic of a high-pressure SFG system, a vibrational spectroscopic tool for probing the adsorbed species during the catalytic reaction. **b**, SFG spectra of adsorbed species on Pt (111) during ethylene hydrogenation under 35 Torr of ethylene, 100 Torr of H₂, and 625 Torr of He. **c**, Schematic of ambient pressure XPS setup at Beamline 9.3.2 of the Advanced Light Source at Lawrence Berkeley National Laboratory. **d**, Evolution of Rh (Rh⁰ + Rh²⁺) and Pd (Pd⁰ + Pd²⁺) atomic fractions in the Rh₀.₅Pd₀.₅ NPs at 300 °C under oxidizing conditions (100 mtorr NO or O₂) and catalytic conditions (100 mtorr NO and 100 mtorr CO) denoted in the x axis. Figures adapted with permission from: **a**, ref. 25, ACS; **b**, ref. 23, Elsevier; **c**, ref. 27, MRS; **d**, ref. 8, AAAS.
Figure 3 | *In situ* characterization of catalysts in decreasing sizes using STM, XPS, NEXAFS, and EXAFS. a, STM images of Pt(557) in increasing pressure of CO from $1 \times 10^{-10}$ Torr to 1 Torr and the corresponding CO coverage determined by APXPS. STM images are 40 nm by 50 nm in size. b, Turnover frequency relative to rhodium foil at 50 Torr O$_2$, 20 Torr CO, at 200 °C, and activation energy (150–225 °C) for CO oxidation. APXPS data show the difference of oxidation state of nanoparticles with 2 nm diameter and 11 nm diameter. c, Top: A scheme based on the XAS results, showing possible structures of the dendrimer-encapsulated Pt catalyst after reduction and oxidation treatment. The gray spheres represent the metallic Pt clusters. The surface Pt chlorides are indicated by red circles. The small blue and green species represent the Pt(II) and Pt(IV) species formed after oxidation treatment. Middle: The fractions of Pt(0) and Pt(II) and Pt(IV) chloride species of the Pt catalyst derived from NEXAFS analysis. Bottom: Average coordination numbers of Pt atoms in the supported Pt catalyst after a sequence of hydrogen reduction and PhICl$_2$ oxidation treatments in the toluene derived from EXAFS analysis. Figures adapted with permission from: a, ref. 33, AAAS; b, ref. 46, Wiley; c, ref. 29, ACS.
Figure 4 | Evidence for the importance of the metal oxide support on catalysis. 

**a**, Left: Schematic of Pt/TiO$_2$ device. Right: Arrhenius plots obtained from chemicurrent and turnover measurements on a Pt/TiO$_2$ diode with pressure of 6 Torr of H$_2$ and 760 Torr O$_2$. Both give similar activation energies, which implies that hot electron generation under hydrogen oxidation is proportional to the catalytic turnover rate. 

**b**, Product distributions of $n$-hexane isomerization over 2.7 nm Pt nanoparticle catalysts supported on different kinds of oxide supports at 360 °C. 

**c**, Schematics of the differences between bifunctional and single-site catalysis. 

**d**, Left: TEM image of Pt/Co$_3$O$_4$ catalysts. Top right: Energy-dispersive spectroscopy (EDS) phase mapping of Pt/Co$_3$O$_4$ catalysts, showing the merged image of the Co K (red) and Pt L (green) lines. Bottom right: High-resolution TEM image of Pt/Co$_3$O$_4$ catalysts. Insert top: Illustration of mesoporous-oxide-supported Pt nanoparticle catalysts. Insert bottom: an illustration showing the potential reaction sites of Pt-nanoparticle-loaded oxide catalysts during CO oxidation. 

**e**, Comparison of TOFs at 473 K of CO oxidation over Pt-nanoparticle-loaded oxide and pure mesoporous oxide catalysts. Figures adapted with permission from: **a** (left), ref. 51, AIP; **a** (right), ref. 53, ACS; **b**, ref. 54, ACS; **d**, **e**, ref. 55, ACS.
Scheme 1 | Schematics showing the evolution of catalyst complexity leading to increased catalytic selectivity for multi-path and multi-product catalytic transformations.